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Evaluation of Wear-Corrosion Synergy Through Tribocorrosion Studies

Suresh Kuiry, PhD

Bruker Nano Surfaces Division

Tribology and Mechanical Testing, 1717 Dell Ave, Campbell, CA 95008, U.S.A.

Introduction

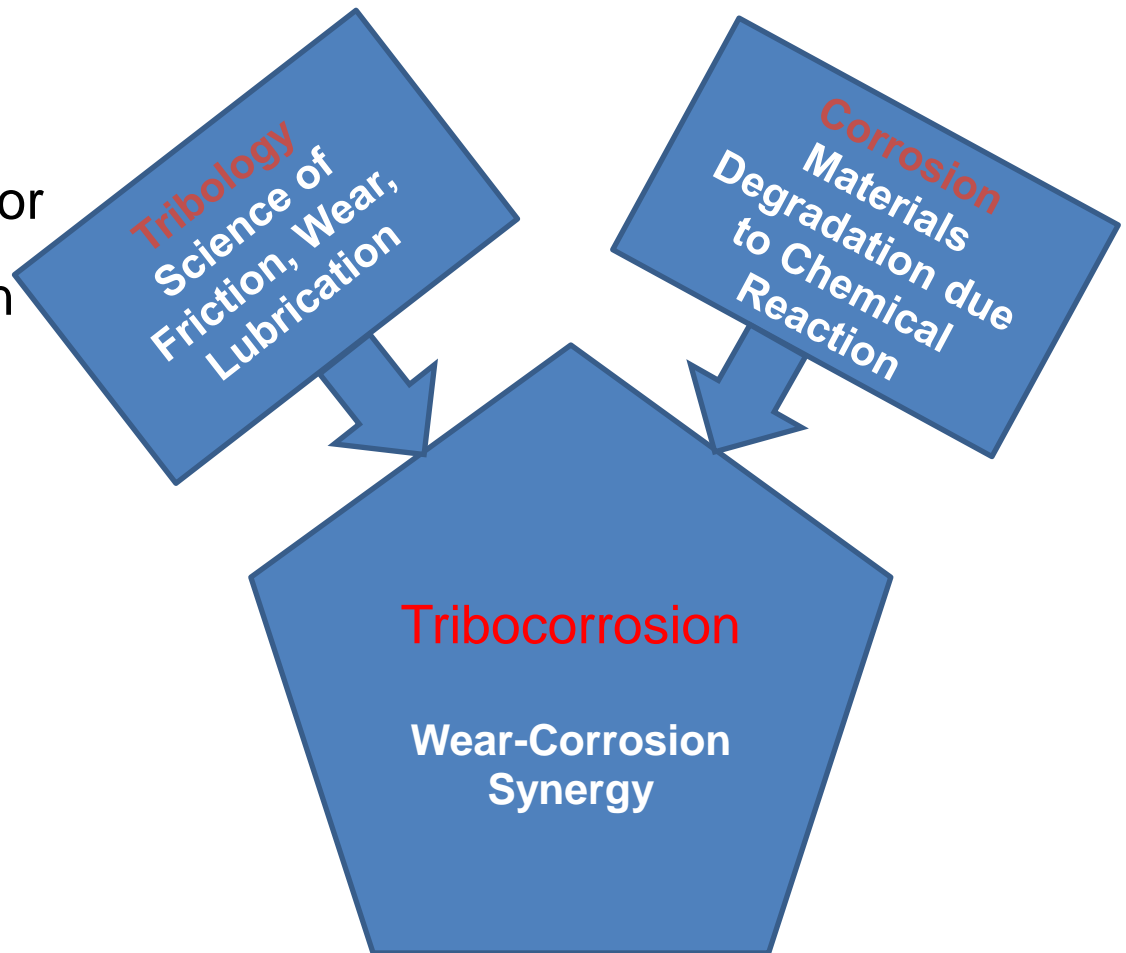


- Tribocorrosion Basics and Applications
- Electrochemical Polarization Methods
- Tribocorrosion Module of CETR-UMT
- Standard Tribocorrosion Test Procedures
- Estimation of Wear-Corrosion Synergy
- Some Test Results Obtained Using CETR-UMT
- Q & A

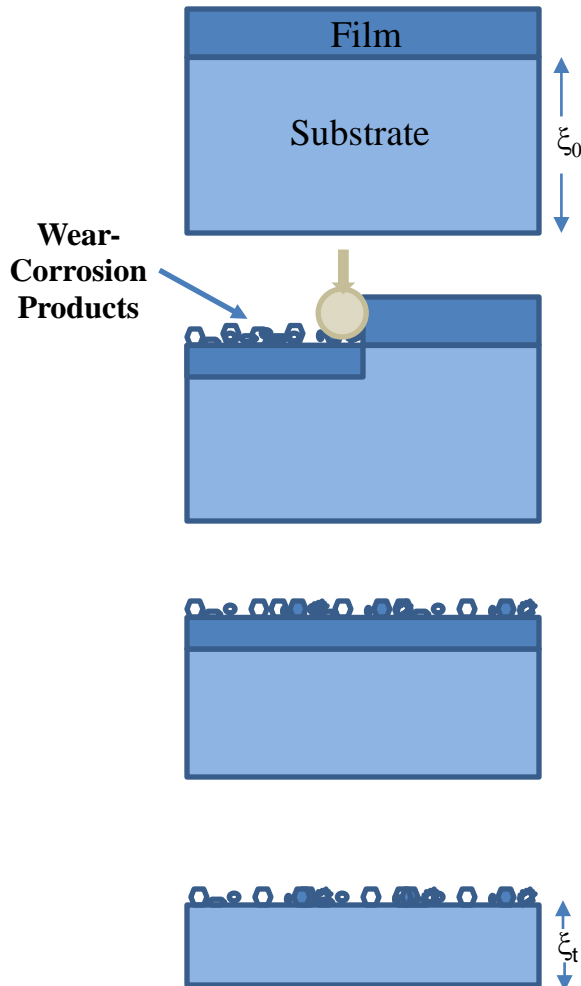
Tribocorrosion



Tribocorrosion involves mechanical and chemical or electrochemical interaction between bodies in relative motion. Mechanical component: *sliding wear, abrasion, cavitation damage, fretting, tribo-oxidation, solid particle erosion* etc.



Wear-Corrosion Synergy



An oxide film protects the substrate from corrosion degradation.

Wear removes the film inducing an accelerated corrosion process

Wear-corrosion products enhance the wear

Huge materials loss due to wear-corrosion synergy

Tribocorrosion-Applications



Automotive: *lubricated moving parts or parts subject to tribo-oxidation*

Biomedical: *interaction of biomedical chemicals on implants*

Chemical, Mining and Petrochemical: *degradation of pumps, valves, propellers, heat exchanger tubes, drilling and slurry transportation*

Dental: *evaluation of degradation of arch-wire, dental implants etc.*

Food: *tribocorrosion of food processing equipment*

Marine: *tribocorrosion in sea water*

Lubricant: *Research and Development of novel lubricants*

Semiconductor: *uses tribocorrosion as a beneficial process (CMP)!!!*

Tools for Tribocorrosion Study



Tribocorrosion study requires a Tribometer and an Electrochemical Measurement System

Tribometer:

- Provides controlled mechanical loading and relative motion;
- Measures friction force and normal force
- Yields evolution of coefficient of friction (COF) with time and materials removal rate.

Electrochemical Measurement System:

- Performs voltage and electrical current application and measurement -open-circuit potential (OCP), Electrochemical polarization, Electrochemical impedance etc.
- Yields corrosion potential and current data (E_{corr} , i_{corr}) and materials removal rate due to corrosion.

Tribocorrosion Tests



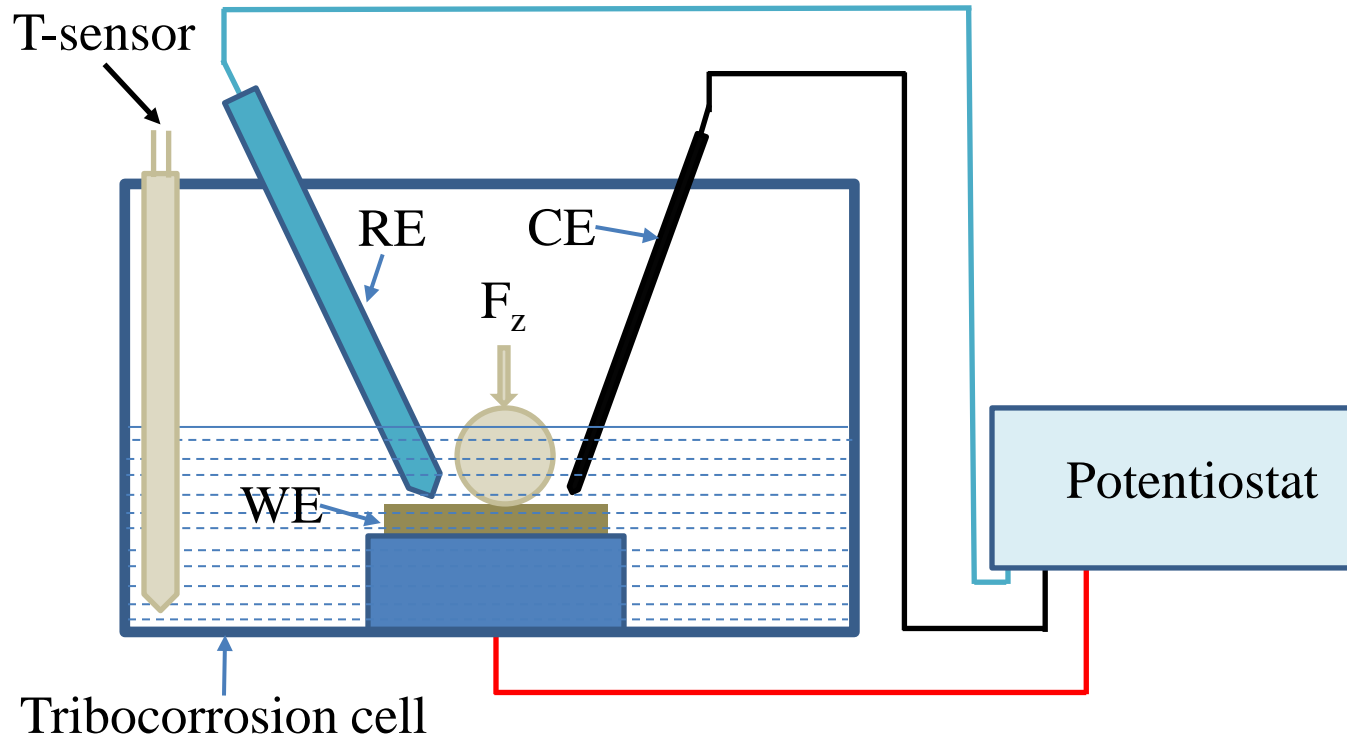
Specimen:

- Bulk or coating of metallic materials (25 mm × 25 mm)
- Chemical solution (acidic, alkaline, oxidants, salt solution, body fluids, ionic lubricants, etc.)

Results:

- Electrochemical Polarization Studies – to evaluate corrosion rate of metals and alloys in chemical environment
- Effect of pH, scan rate, electrolyte concentration, temperature on wear behavior of metallic materials
- Synergistic effect of wear and corrosion

Schematic Tribocorrosion Cell



WE: Working Electrode- metallic specimens;

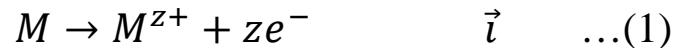
CE : Counter Electrode (Pt)

RE : Reference Electrode-Ag/AgCl, calomel electrode, etc

Electrochemical Kinetics



Metal dissolution reaction :



Metal deposition reaction:



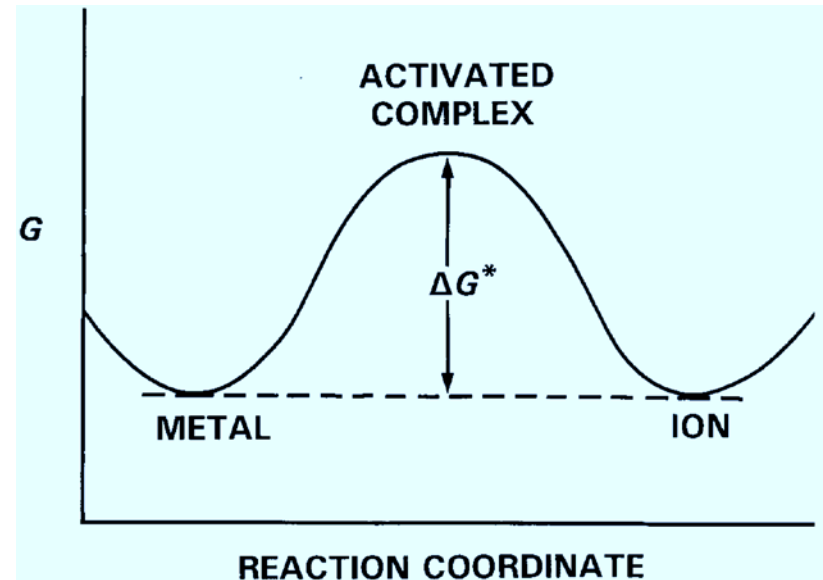
At equilibrium, the magnitude of the partial currents (\vec{i} and \vec{i}) is called the exchange current density (i_0), which is a function of activation free energy (ΔG^*):

$$i_0 = \vec{i} = \vec{i} = k \exp \frac{-\Delta G^*}{RT} \quad \dots(3)$$

k is a constant, R is the universal gas constant, T is temperature

$$\Delta G^* = -zFE^* \quad \dots(4)$$

F is Faraday charge (96,490 Coulomb/mol). At equilibrium no net current flows.



Electrochemical Polarization

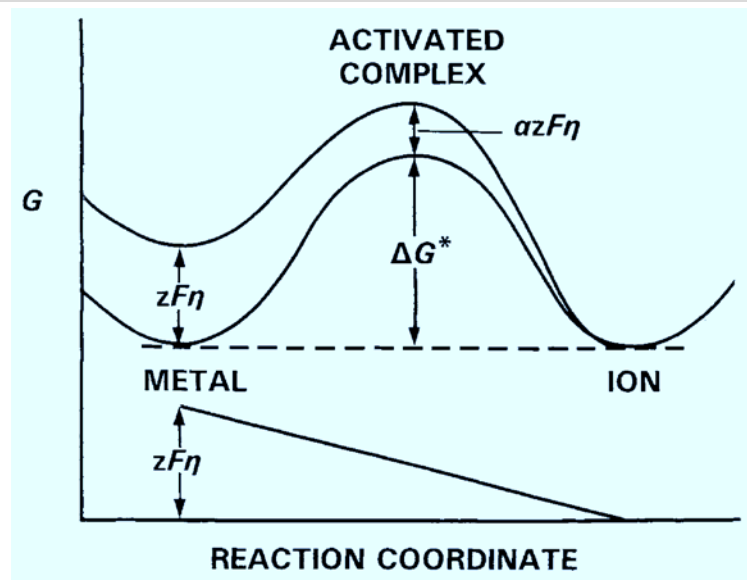


If the equilibrium at an electrode is disturbed, a net current flows across its surface that shifts the potential. The shift in potential is called the *polarization* and its value is overpotential (η).

Three types of polarization:

- (a) *activation*
- (b) *concentration*
- (c) *resistance*

Activation polarization: anodic when it is +ve; cathodic when -ve.



The free energy profile of an electrode that is subjected to an anodic polarization with an overpotential (η) is shown. It raises the energy of the metal by $zF\eta$ and that of the activated complex by $\alpha zF\eta$, relative to that of the ions, where α is a symmetry factor ($0 < \alpha < 1$) defining the position of the maxima in the energy profile. Therefore,

The activation energy of metal dissolution is decreased to $[\Delta G^* - (1-\alpha)zF\eta]$, and

the activation energy for metal deposition is increased to $[\Delta G^* + \alpha zF\eta]$.

Butler-Volmer Equation



Under anodic polarization condition, metal dissolution current (\vec{i}) [eqn (3)] is changed to :

$$\vec{i} = k \exp \frac{-\{\Delta G^* - (1-\alpha)zF\eta\}}{RT} \quad \dots(5)$$

$$\vec{i} = k \exp \frac{-\Delta G^*}{RT} \cdot \exp \frac{(1-\alpha)zF\eta}{RT} \quad \dots(6)$$

$$\vec{i} = i_0 \cdot \exp \frac{(1-\alpha)zF\eta}{RT} \quad \dots(7)$$

Similarly, deposition current (\vec{i}):

$$\vec{i} = i_0 \cdot \exp \frac{-\alpha zF\eta}{RT} \quad \dots(8)$$

The net anodic (dissolution) current (i_{net}) is obtained by subtracting (8) from (7):

$$i_{net} = \vec{i} - \vec{i} = i_0 \cdot \left[\exp \frac{(1-\alpha)zF\eta}{RT} - \exp \frac{-\alpha zF\eta}{RT} \right] \quad \dots(9)$$

The equation (9) is known as the **Butler-Volmer** equation that relates i_{net} with η .

Tafel Equation



For high-field approximation, when anodic overpotential [$\eta = \eta_{\text{anodic}}$] is > 0.1 V, metal deposition reaction is insignificant, and i_{net} from eqn (9) becomes:

$$i_{\text{net}} = \vec{i} = i_{\text{anodic}} = i_0 \cdot \left[\exp \frac{(1-\alpha)zF\eta_{\text{anodic}}}{RT} \right] \quad \dots(10)$$

The equation (10) can be expressed as :

$$\eta_{\text{anodic}} = b \cdot \log(i_0) + \beta_a \cdot \log(i_{\text{anodic}}) \quad \dots(11)$$

Similarly, for higher cathodic overpotential [$\eta = \eta_{\text{cathodic}} < -0.1$ V], metal dissolution reaction is insignificant, and i_{net} from eqn (9) could be expressed as:

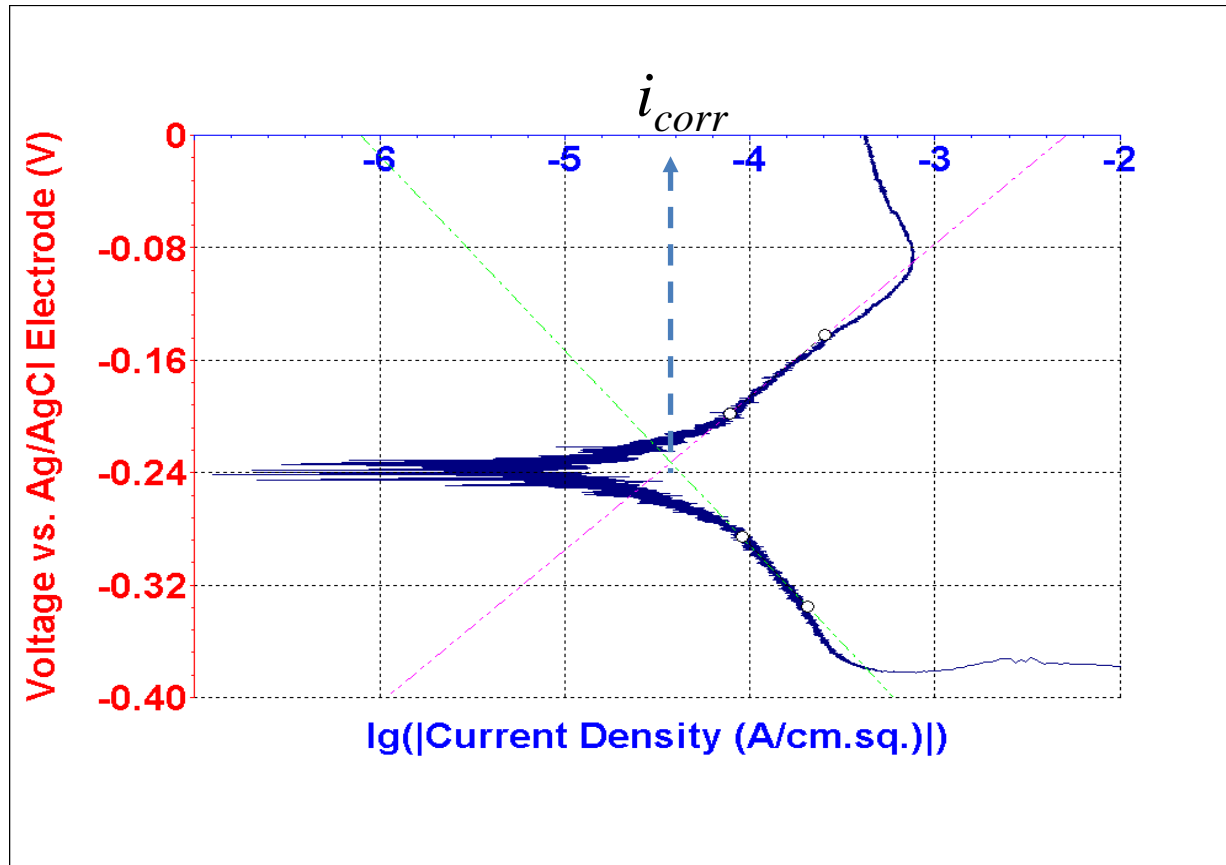
$$\eta_{\text{cathodic}} = b \cdot \log(i_0) - \beta_c \cdot \log(i_{\text{cathodic}}) \quad \dots(12)$$

Equations (11) and (12) are combined into a single expression and known as Tafel equation:

$$\eta = b \cdot \log(i_0) \pm \beta \cdot \log(i) \quad \dots(13)$$

The symmetry factor α is usually 0.5.

Tafel Extrapolation



Corrosion rate = $k_1 \frac{i_{corr}}{\rho} EW$, where, ρ and EW are the density and the equivalent weight of the metallic specimen, respectively.

CETR-UMT: Tribocorrosion Tester



- Up to 20 N normal load (Fz)-servo controlled-programmable
- Ball or pin-on-Plate wear test up to 30 Hz
- 3-electrode (counter, working, ref.) system
- Potentiostat
- Temperature up to 70 °C
- Corrosion resistant Tribocorrosion cell
- Tests as per ASTM standards



CETR-UMT Tribocorrosion Module





ASTM G119

Wear and Corrosion form a Synergistic Couple!

$$T = W_0 + C_0 + S \quad \dots(14)$$

T = Rate of total material loss due to tribocorrosion

W_0 = Rate of mechanical wear in absence of corrosive agent

C_0 = Rate of corrosion in absence of mechanical agent

S = Change in rate of materials loss due to wear-corrosion synergy

Evaluation of Wear-Corrosion Synergy



To obtain Synergy (S), the following tests are performed:

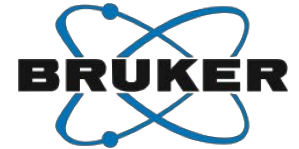
Test 1: Electrochemical polarization to find corrosion potential (E_{corr}) and corrosion current (i_{corr}) to calculate C_0

Test 2: Wear test in corrosive environment; No external potential or electrical current to obtain T .

Test 3: Repeat Test 2 to obtain electrochemical corrosion rate in the presence of wear (C_w)

Test 4: Repeat Test 2 with a potential 1V cathodic to E_{corr} to obtain W_0

Evaluation of Wear-Corrosion Synergy



$$T = W_0 + C_0 + S \quad \dots(14)$$

where,

$$S = \Delta C_W + \Delta W_C \quad \dots(15)$$

and

$$\Delta C_W = C_W - C_0 \quad \dots(16)$$

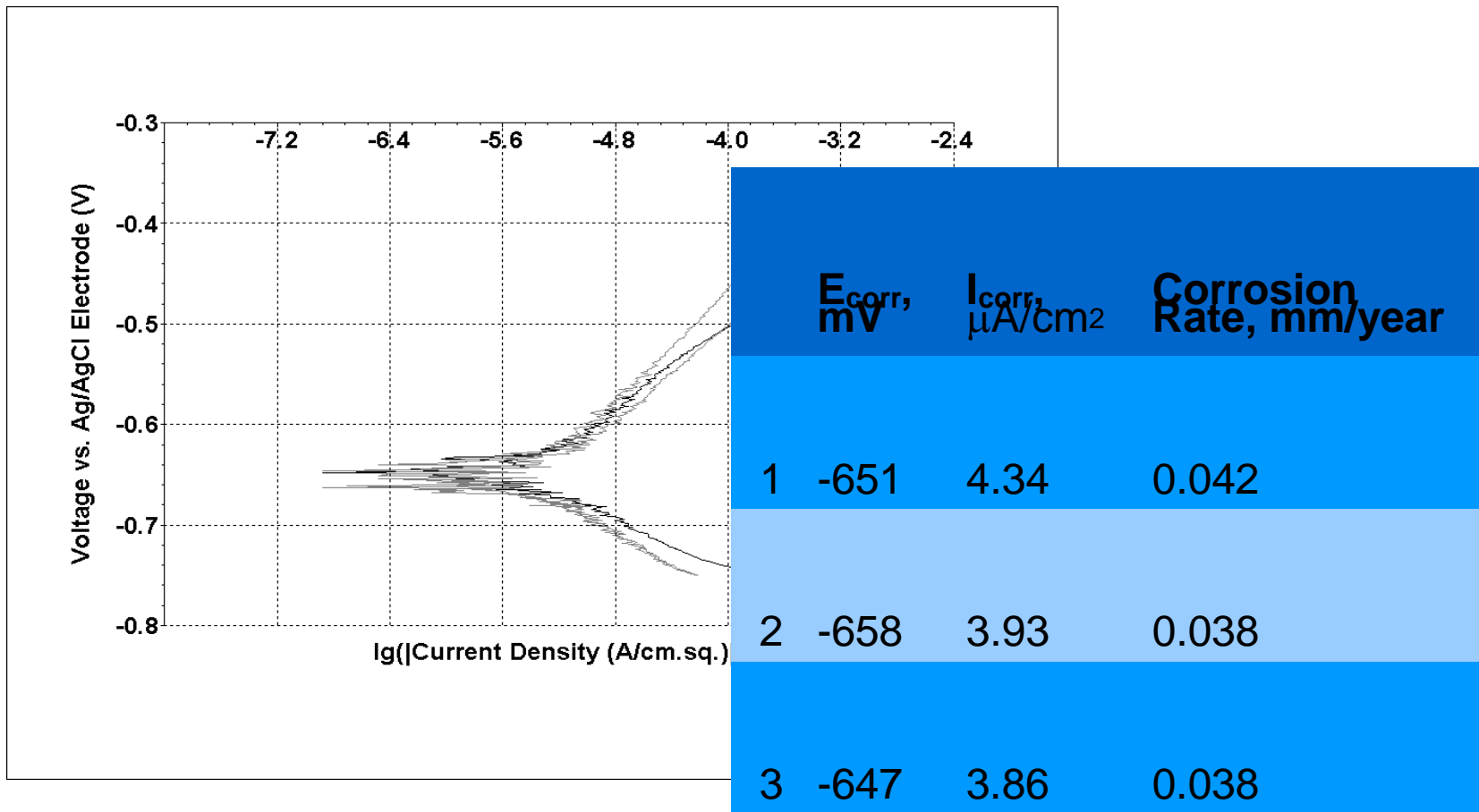
$$\Delta W_C = T - (W_0 + C_W) \quad \dots(17)$$

$$\text{Total Synergism Factor} = \frac{T}{(T-S)} \quad \dots(18)$$

$$\text{Corrosion Augmentation Factor} = \frac{C_W}{C_0} \quad \dots(19)$$

$$\text{Wear Augmentation Factor} = \frac{W_0 + \Delta W_C}{W_0} \quad \dots(20)$$

Electrochemical Corrosion Rate

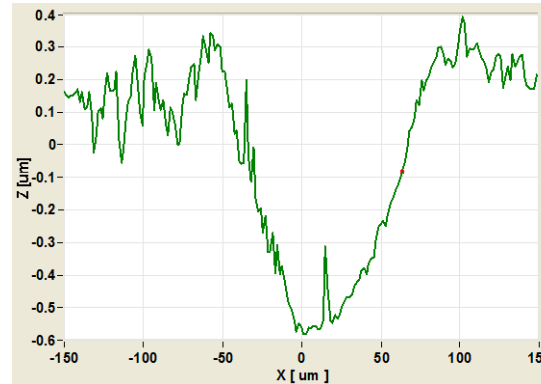
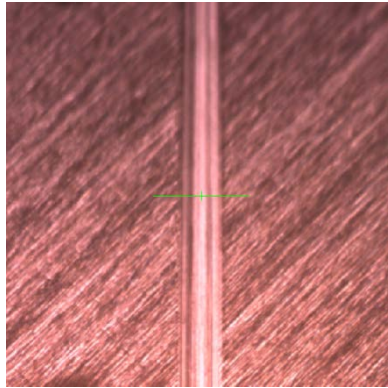


Cast iron in 0.1% NaCl solution

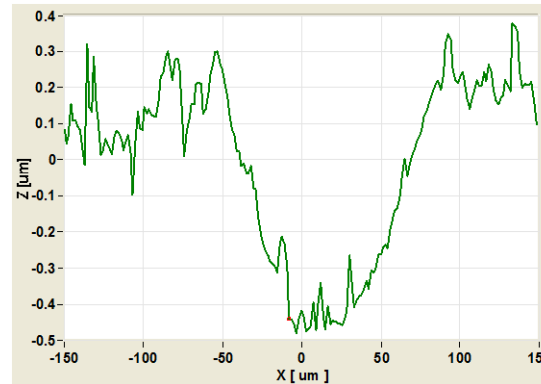
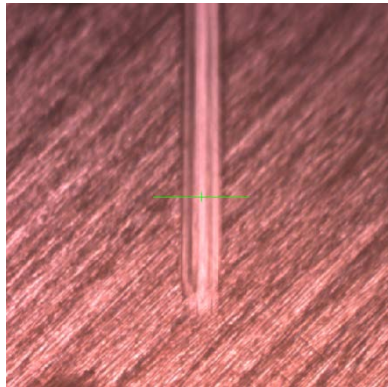
Wear Scar Profile after Tribocorrosion



Near the Middle



Near an End



AISI 316 SS in 0.9%NaCl; 900 s with 5 N load with alumina-4.75 mm ϕ ball and reciprocation over 2 mm at 0.4 mm/s.

Wear-Corrosion Synergy Results



Materials Removal Rate of AISI 316 SS in 0.9%NaCl with 5N load, 0.4 mm/s with alumina ball (4.76 mm dia) in mil per year (mpy):

$$T = 117.82; W_0 = 18.77;$$

$$C_W = 0.55; C_0 = 0.31$$

$$\Delta C_W = C_W - C_0 = 0.24;$$

$$\Delta W_C = T - (W_0 + C_W) = 98.50;$$

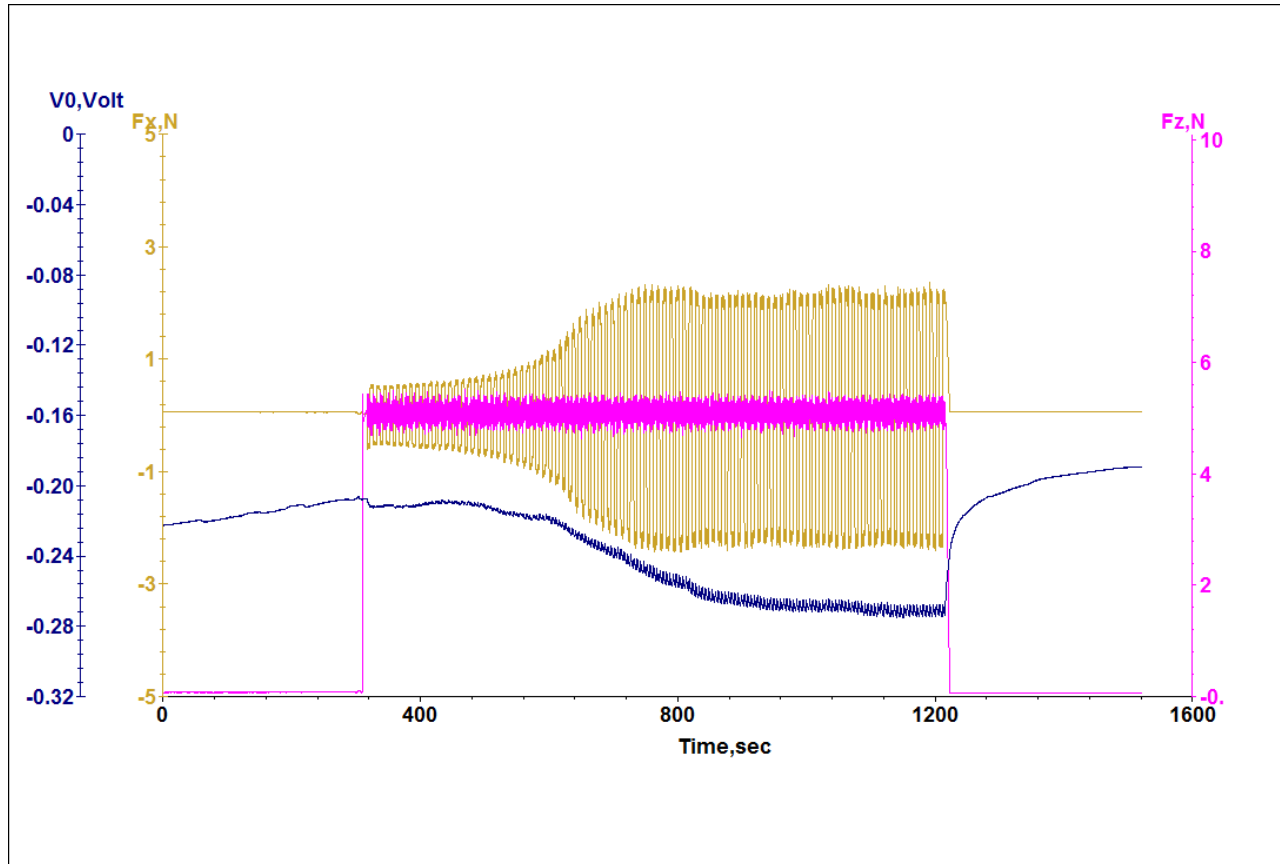
$$S = \Delta C_W + \Delta W_C = 98.74.$$

$$\text{Total Synergism Factor} = \frac{T}{(T-S)} = 6.18$$

$$\text{Corrosion Augmentation Factor} = \frac{C_W}{C_0} = 1.77$$

$$\text{Wear Augmentation Factor} = \frac{W_0 + \Delta W_C}{W_0} = 6.25$$

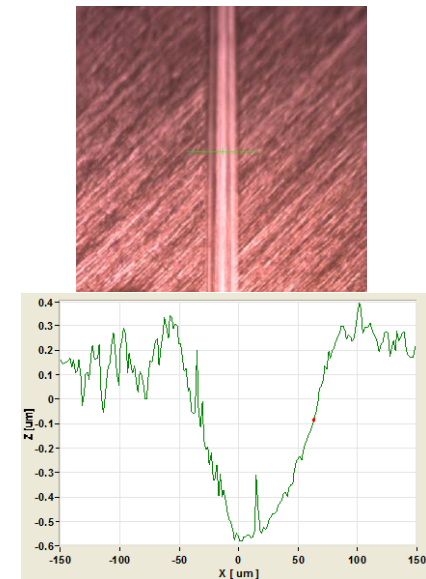
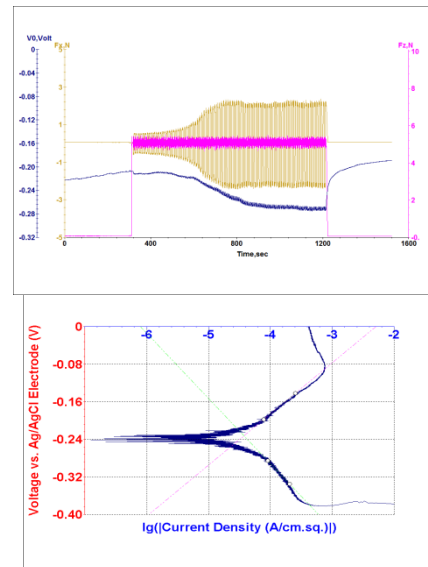
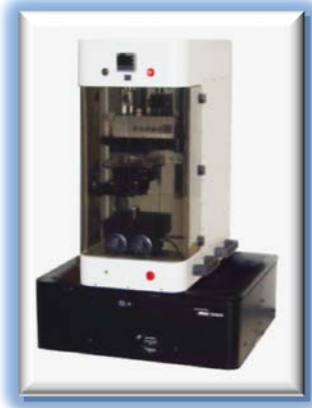
Tribocorrosion Test: OCP Results

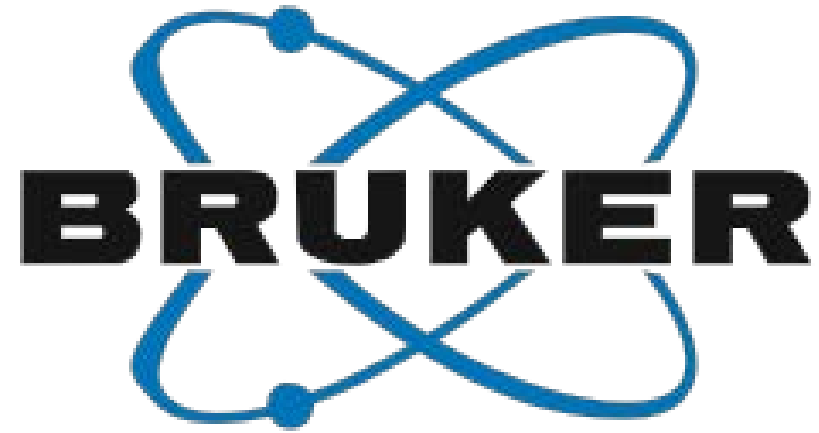


AISI 316 SS in 0.9%NaCl; initial 300 s no load- no movement; next 900 s with 5 N load with alumina-4.76 mm ϕ ball and reciprocation over 2 mm at 0.4 mm/s; Next 300 s load removed and movement stopped.

Concluding Remarks

- Tribocorrosion test procedure is important to evaluate metallic materials or solution for their performance under simultaneous wear and corrosion conditions.
- CETR-UMT Test system can evaluate Wear-Corrosion Synergy of an electrochemical system involving chemicals and metallic materials including coatings.





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